

wherein

$R^1$  and  $R^2$  are independently H,  $-CH_3$ ,  $-C_2H_5$ ,  $-C_3H_7$  or together form  $-(CH_2)_n-CH_2-$ ;

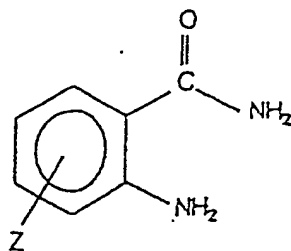
X is  $-CH_2$ , CO, or CS;

Y is S, NH, or  $-(CH_2)_m-$ ;

n is 0 to 9

m is 1 to 4;

and a compounds of formula (II)



wherein

Z is  $-OCH_3$ ,  $-SO_3H$ ,  $-SO_3^+M^+$ ,  $-NO_2$ ,  $-NH_2$ ,  $-NH-NH_2$ ,  $-CO_2^+M^+$ ,  $-CHO$ , or H

M is a cation;

wherein the molar ratio of amino resin former : formaldehyde : sulfite: nitrogen-containing formulation auxiliary is 1 : 1.9 – 6.0 : 1.0 – 2.0 : 0.01 – 1.5 and/or the molar ratio of naphthalene-sulfonic acid : formaldehyde : nitrogen-containing formulation auxiliary is 1 : 0.7 – 3.0 : 0.01 – 1.5.

14. A condensation product as claimed in claim 13, wherein said amino resin former is selected from the group consisting of melamine and urea.

15. A condensation product as claimed in claim 13, wherein said formulation auxiliary is selected from the group consisting of urea, thiourea, N-methylurea, 2-imidazolidinone and anthranilamide as formulation auxiliaries.

16. A condensation product as claimed in claim 13, wherein the amino resin former comprises up to 70% by weight of thiourea, dicyandiamide, a guanidine (salt) or mixtures thereof.

17. A condensation product as claimed in claim 13, wherein the condensation product is an aqueous solution having a solids content of from 20 to 60% by weight.

18. A condensation product as claimed in claim 17, wherein the viscosity of the aqueous solution at 95°C is from 0.5 to 250 mm<sup>2</sup>.s<sup>-1</sup>.

19. A condensation product as claimed in claim 13, wherein the aqueous solution has been dried to a residual moisture content of < 5%.

20. A process for preparing a condensation product as claimed in claim 13, comprising:

- a) heating said amino resin former or formers, said formaldehyde and said sulfite component in a molar ratio of 1 : 1.9 – 6.0 : 1.0 – 2.0 in aqueous solution with addition of a portion of the selected molar amount of the formulation auxiliary at a temperature of from 40°C to 90°C and a pH of from 7.5 and 13.0 until sulfite is no longer detectable;
- b) adding a portion 2 of the selected molar amount of the formulation auxiliary at a pH of from 3.0 to 7.0 and continuing the condensation at a temperature of from 60 to 95°C until the condensation product has a viscosity at 95°C of from 1 to 250 mm<sup>2</sup>.s<sup>-1</sup>;
- c) adding the pH of condensation product to a pH of from 7.5 to 12.0 or conducting a thermal after-treatment at a pH of  $\geq$  10.0 and a temperature of from 65 to 90°C; and

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d) adding a portion 3 of the selected molar amount of the formulation auxiliary;

wherein the sum of portion 1, portion 2 and portion 3 of the formulation auxiliary corresponds to the molar amount of the formulation auxiliary of the formula (I) and/ (II) and each individual portion can amount to a proportion of from 0 to 100 total-%, wherein portion 1 is < 100%.

21. The process as claimed in claim 20, wherein the resultant condensation products are dried in a spray drier or on a roller drier to a preferred residual moisture content of < 5% by evaporation of the water under reduced pressure.

22. A process for preparing a condensation product as claimed in claim 13, wherein the sulfonated melamine-formaldehyde condensation products, sulfonated melamine-urea-formaldehyde condensation products or naphthalenesulfonic acid-formaldehyde condensation products are admixed with from 0.1 to 50% by weight, based on the content of solid active components, of a formulation auxiliary of the formula (I) and (II) or mixtures thereof and dried to a residual moisture content of < 5%.

23.. An inorganic binders comprising from 0.01 to 20% by weight of condensation product as claimed in claim 13, based on the amount of the inorganic binders.

24. An hydraulically setting dry mixes comprising from 0.01 to 20% by weight, of a condensation product as claim in claim 13, based on the amount of inorganic binders.